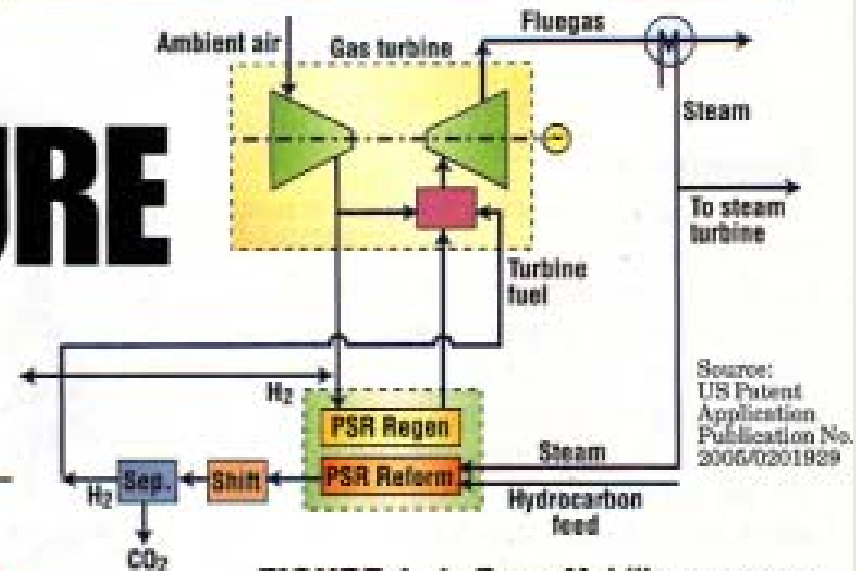


# 5°) carbon capture and storage

# CARBON CAPTURE AND STORAGE

Whether a CPI company's interest is based on reducing its own CO<sub>2</sub> emissions or supplying technology to curb that of its potential customers, this growing field has implications for all

Michele M. Glessner and Jeffrey E. Young, Alston & Bird



**FIGURE 1.** In ExxonMobil's process, a hydrocarbon feed such as methane and steam are passed through a pressure-swing reformer (PSR) and converted to synthesis gas. In a shift reactor, the CO in the synthesis gas is converted to CO<sub>2</sub> and a hydrogen-enriched gas stream is produced. Hydrogen is separated from the CO<sub>2</sub> in a separation zone and used as fuel for a gas turbine

# CO<sub>2</sub> A RAW MATERIAL FOR SUSTAINABLE DEVELOPMENT

## Cost of CO<sub>2</sub> from adsorption processes

(NH<sub>3</sub>, MEA, Na<sub>2</sub>CO<sub>3</sub> powder, zeolithe beads, cryogenic route)

between 20 – 60 \$/T

(MIT evaluation science 27.02.09)

## Investment for CO<sub>2</sub> adsorption on coal power unit of 1000 MW

---

**1 – 2 billion\$**

Purity of CO<sub>2</sub> from adsorption processes      99 %

Questions: CO<sub>2</sub>

→ Waste or raw material ?

European Parlemnt STOA 22 /3/2011

→ New industrial processes ?

# technical aspects of the industrial CO<sub>2</sub> capture units

- gas- liquid adsorption systems
- gas\_solid adsorption systems
- gas- liquid transformation through cryogenic process

# carbone dioxide capture

European Parlement and European Commission have launched a program for CO2 sequestration

STOA 2005-28 and 2008-01, and European set plan

A new control of the gas out put from burning system

° -Dow –Alstom (pilot plant 1800 T/Y) Dow'south Charleston W.Va)-amine CO2 removal

° -Alstom-Polish utility PGE Electrownia Belchatow (100.000T/Y) amine removal

° -Air products CCS demonstration in Schwarze Pumpe Germany built by Alstom operated by Swedish utility Vattenfall

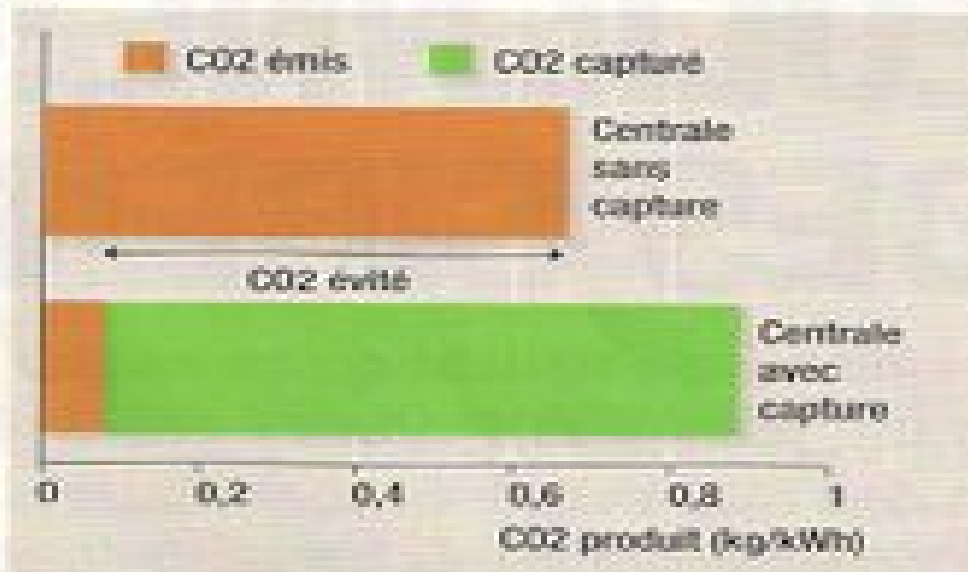
- Siemens with aquaous amino acid salt solution ( ACS news 2011)

Le gaz à effet de  
sera produit par  
de moyens de  
en France,  
industrie lourde.



Le CO<sub>2</sub> est alors séparé de l'hydrogène, lequel peut être utilisé pour produire de l'énergie (électricité et ou chaleur) sans émission de CO<sub>2</sub>.

Pour chacune des 3 grandes voies de captage il y a donc, à un moment donné, une séparation gazeuse : H<sub>2</sub>/CO<sub>2</sub> (post-combustion), O<sub>2</sub>/H<sub>2</sub> (oxycombustion) et CO<sub>2</sub>/H<sub>2</sub> (pré-combustion). On dispose de tout un ensemble de technologies de séparation gazeuse. Certaines existent à l'échelle industrielle, d'autres ne sont disponibles qu'au laboratoire et nécessitent la réalisation de démonstrateurs. Toutes font encourir une pénalité énergétique qu'il faut réduire.



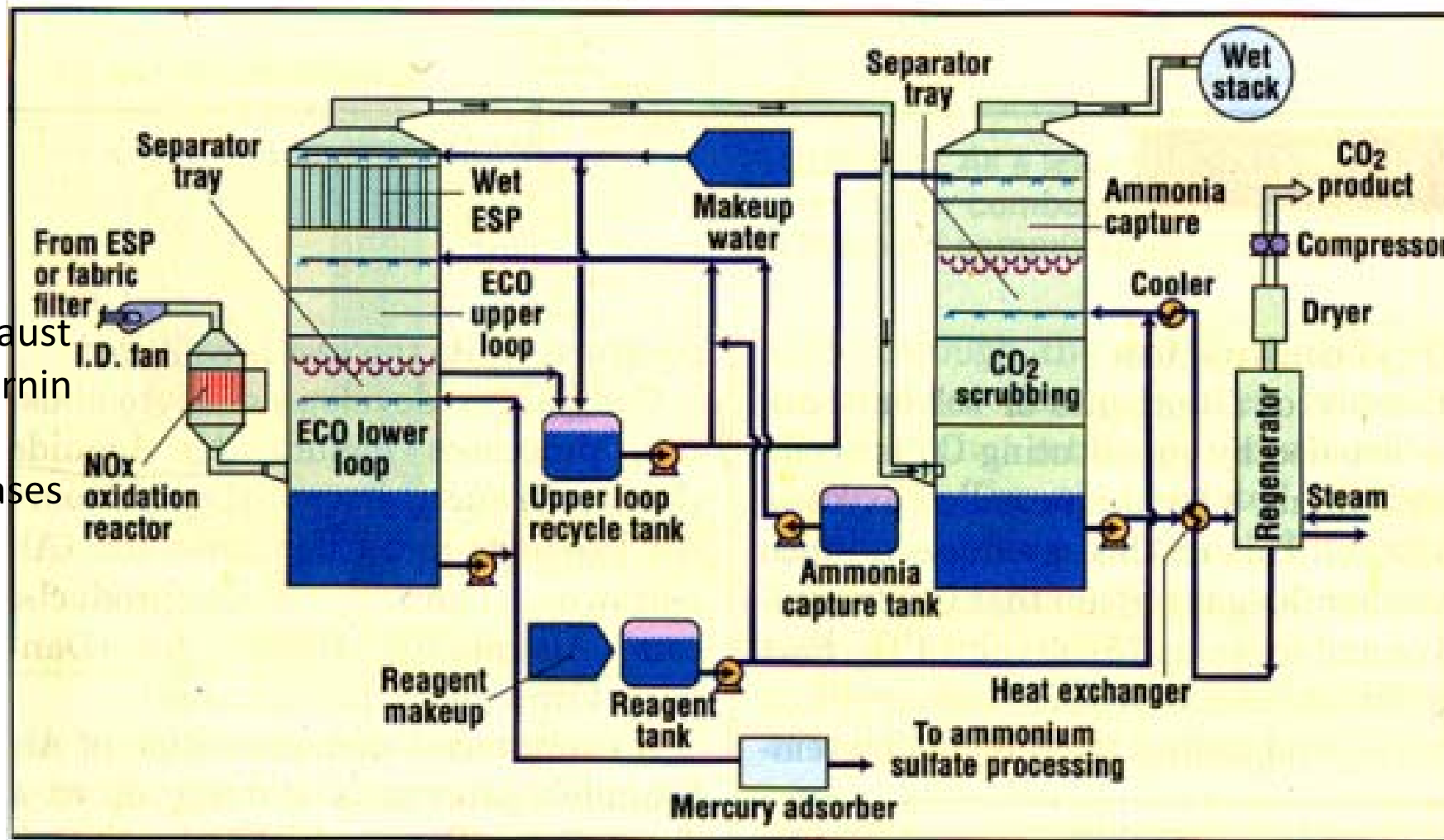
# Main Financial Aspects of the EEC

- In order to start the capture of CO<sub>2</sub> ( CCS) the EEC has been decided to develop 10 industrial 1000MW coal power plants for learning step
- total amount of 12 billions euros
- goal: the scale up of that kind of industry
- For each plant :a capture of 5 millions tons of CO<sub>2</sub> per year and cost 200 euros/T
- 2020 the goal is 300 CCS industrial Plants

# CAPTURING CO<sub>2</sub>

:Ammonia process

Efforts to find economical technology to reduce CO<sub>2</sub> emissions are intensifying

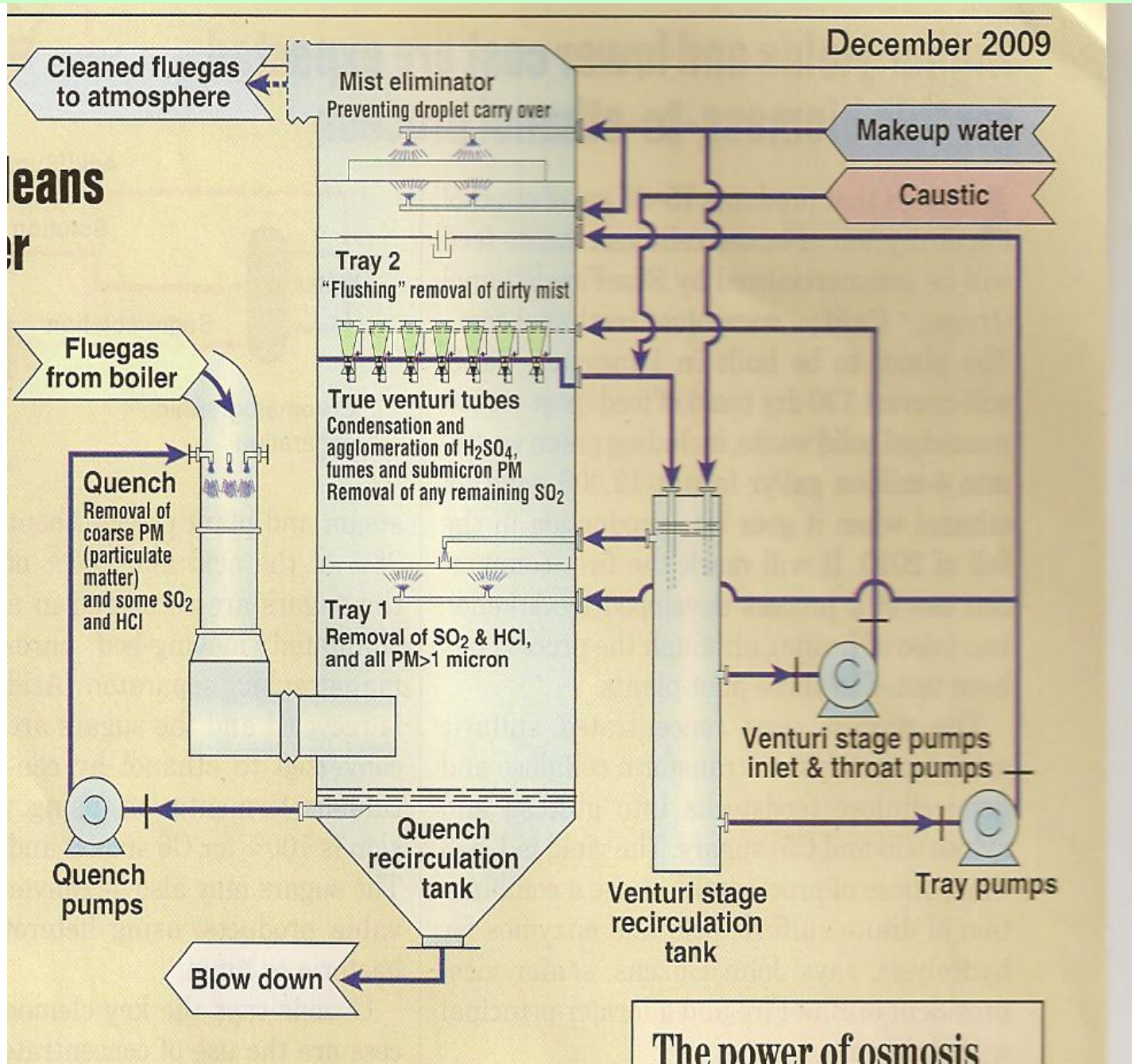


**FIGURE 1.** In this integrated version of Powerspan's ECO and ECO<sub>2</sub> processes, ammonia is recycled from the ECO<sub>2</sub> CO<sub>2</sub> absorber to scrub SO<sub>2</sub> in the ECO process

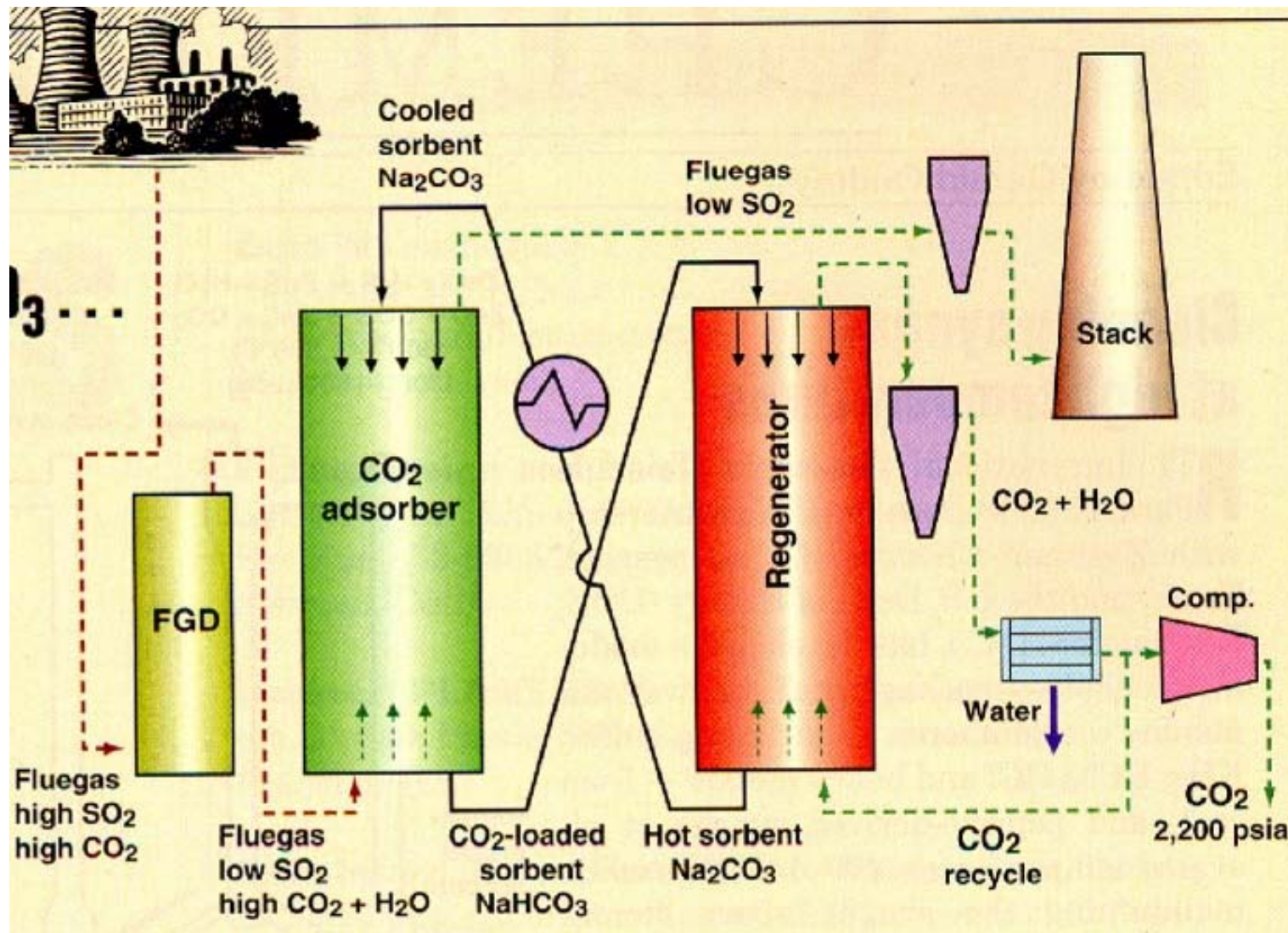
Chemical Engineering, Dec. 2003, p. 17, Power span Conf. Portsmouth, NH, USA



# gas combustion cleaning before carbon dioxide adsorption



# Two solid ways to remove CO<sub>2</sub> from fluegas, one based on Na<sub>2</sub>CO<sub>3</sub>.



**CCS NH3  
développé  
par ALSTHOM  
/USA**

opment for Alstom.  
er the CO<sub>2</sub> is cap-  
Hilton says, the  
ing mixture is then  
ed to a regenerator.  
it is heated to more  
00 °C, and the bicar-  
everts to carbon-  
l to CO<sub>2</sub>, which is  
trated under pres-  
he intended result  
h-pressure, 90%-  
ream of CO<sub>2</sub> and  
aration of ammonia  
se.

CO<sub>2</sub> capture system  
ot of energy, and  
s target is to get  
rgy use of the col-  
system down to  
of a plant's total  
If successful, Al-  
edicts, the system  
up the cost of elec-  
76 to 9 cents per  
-hour—approxi-

oubling the current cost per kilowatt-hour.  
as also joined in the technology development  
and is working with Alstom to develop an ad-  
mine-scrubbing technology.

nding on results, the trial may grow. American  
Power and Alstom plan to install the technol-

ogy later this year at AEP's New  
Haven, W.Va., electric plant and



WE ENERGIES (BOTH)

*A consortium of investors have high hopes that a test at We Energies' 1,210-MW plant will remove CO<sub>2</sub> efficiently and inexpensively.*



# Commercial Demonstration of Ammonia CO<sub>2</sub> Capture

- Flue gas stream for 120 MW
- 1 million tons CO<sub>2</sub> removed
- \$200 to \$300 million in capital
- \$25 to \$35 per ton CO<sub>2</sub>

Gary Loop



*Antelope Valley  
Station (AVS)*

European Parliament STOA 22 /3/2011  
EMRS/UPMC

EMRS Fall Meeting  
Warsaw 13-15 sept 2010  
Symposium A

## SEEKING PATENTS ON ASPECTS OF CO<sub>2</sub> CAPTURE

Invention title	Patent or published application	Owner
Method and apparatus for efficient injection of CO <sub>2</sub> in oceans	6,598,407	UT-Battelle, LLC
Device for removing carbon dioxide from exhaust gas	7,022,168	Alstom Technology LTD
Method for recycling carbon dioxide for enhancing plant growth	6,237,284	The Agricultural Gas Co.
Integration of hydrogen and power generation using pressure swing reforming	2005/0201929	ExxonMobil Research and Engineering
Removal of carbon dioxide from air	2006/0186562	Wright, et. al.
Efficient combined cycle power plant with CO <sub>2</sub> capture and a combustor arrangement with separate flows	2006/0112696	Statoil ASA
System and method for combined microseismic and tiltmeter analysis	2006/0081412	Pinnacle Technologies, Inc.

CHEMICAL ENGINEERING [WWW.CHE.COM](http://WWW.CHE.COM) MAY 2008

## SIEMENS CLAIMS CO<sub>2</sub> REDUCTION ADVANCE

Siemens Energy claims that its CO<sub>2</sub> reduction technology has achieved a CO<sub>2</sub> capture efficiency of more than 90% in a pilot facility at a power plant owned by the firm E.ON

SIEMENS

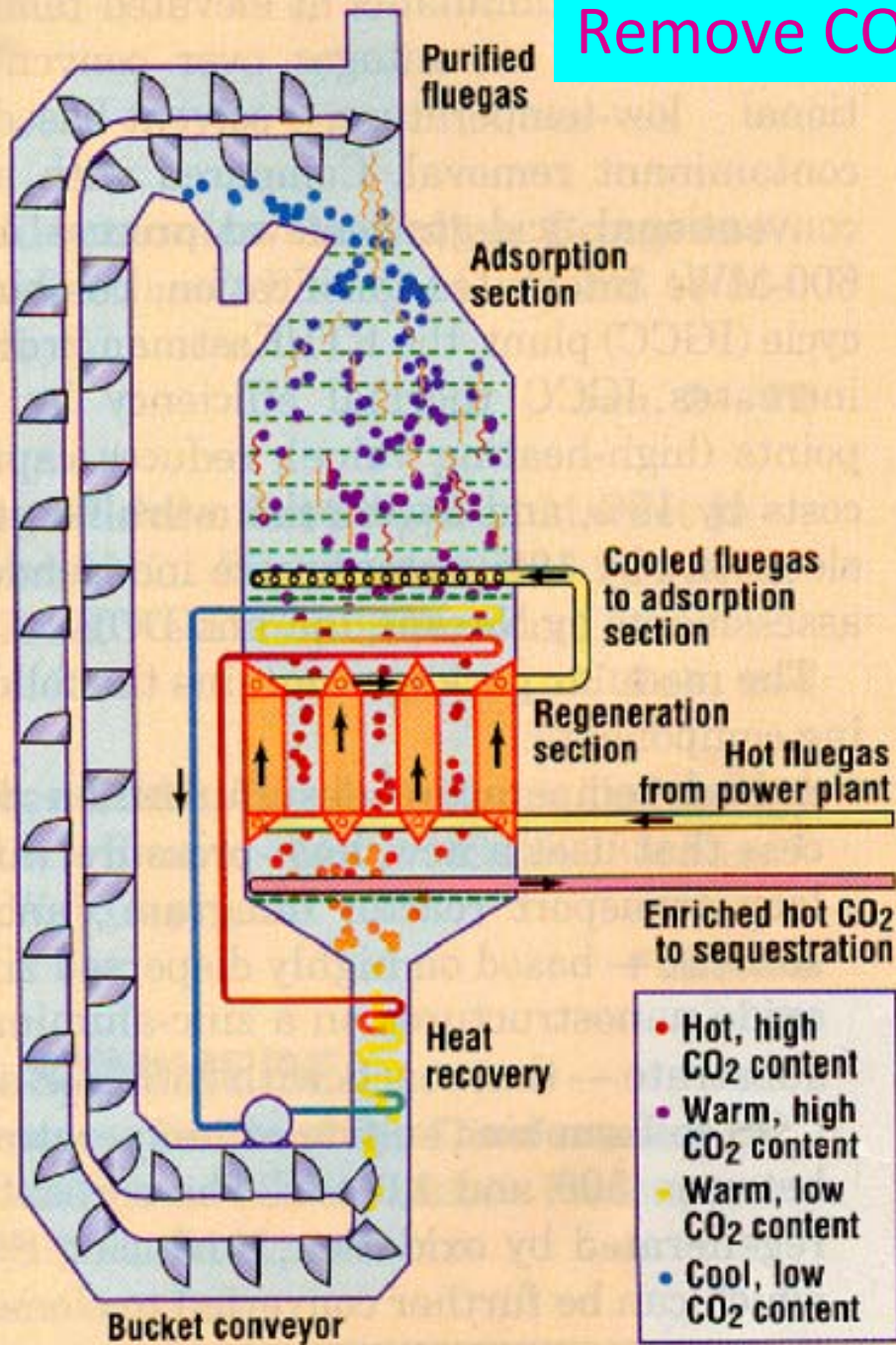


*Workers confer inside the CO<sub>2</sub> capture facility at E.ON's power plant near Hanau, Germany.*

near Hanau, Germany. Siemens says its scrubbing agent, an aqueous amino acid salt solution, provides better energy efficiency than amine-based agents offered by firms such as Dow Chemical and BASF. And because the salt is nonvolatile, practically no solvent emissions need to be scrubbed from power plant flue gas, Siemens says.—MM



## Remove CO<sub>2</sub> with adsorbing beads



In a concept being developed by Adsorption Research, Inc. (ARI; Dublin, Ohio; [www.adsorption.com](http://www.adsorption.com)), adsorbent beads are delivered to the top of an adsorber column by a bucket elevator and fall down through an adsorption section, counter to upflowing, cooled fluegas. The beads' passage is slowed by a series of perforated trays to provide a residence time of about 1-1/2 min for carbon dioxide adsorption.

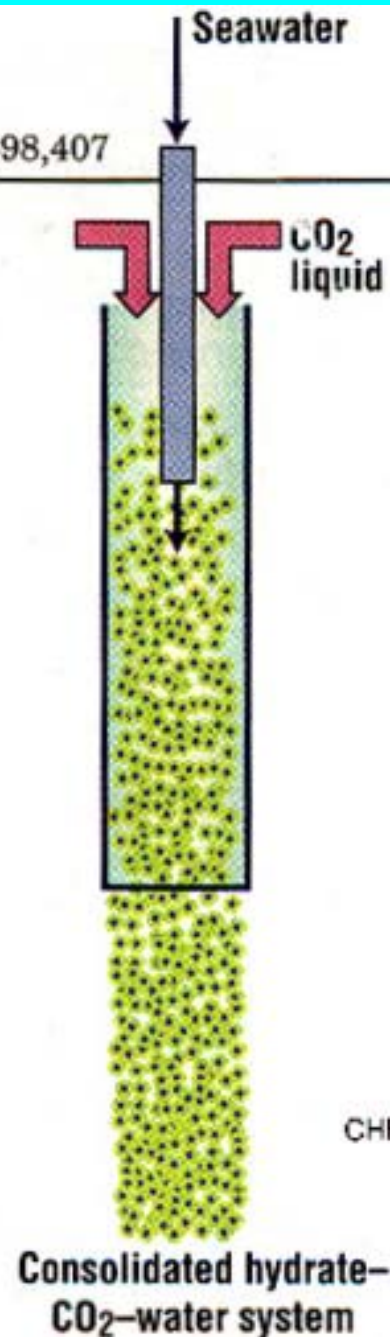
Next, the beads drop through a heat-exchanger section, where they are indirectly heated to 400–600°F by incoming fluegas. The heat releases the CO<sub>2</sub>, which is withdrawn through a perforated pipe. Simultaneously, the gas is cooled to about

125°F for the adsorption step.

In laboratory tests, using a zeolite or a proprietary adsorbent, the process has achieved 89% CO<sub>2</sub> recovery, with a purity of 99%, says Kent Knaebel, president of ARI. He adds that, unlike MEA adsorption, the process requires little parasitic heat or cooling energy and the adsorbent is not degraded by SO<sub>2</sub>, NO<sub>x</sub> or O<sub>2</sub>. He estimates that a commercial unit could process 15,000 tons/d of CO<sub>2</sub> from a 500-MW power plant for under \$20/ton, compared with about \$40/ton for MEA.

# Mixing sea water and CO<sub>2</sub> for sequestration

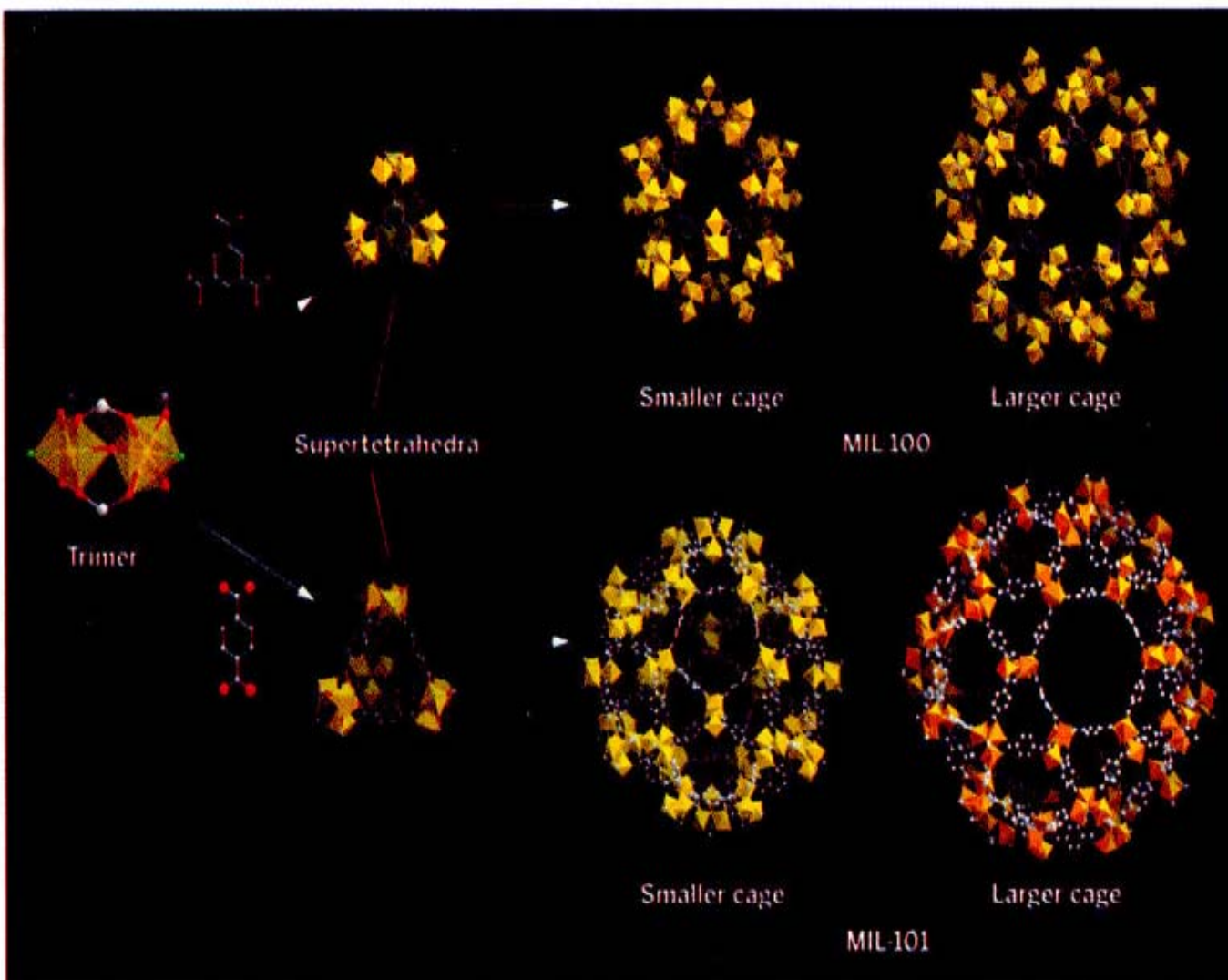
Source: U.S. Patent No. 6,598,407



**FIGURE 2.** UT-Battelle's method of mixing seawater and CO<sub>2</sub> is claimed to increase efficiency, increase the residence time of CO<sub>2</sub> in the ocean, and decrease the cost of CO<sub>2</sub> sequestration, while reducing the negative effects of simply releasing CO<sub>2</sub> gas into ocean water

CHEMICAL ENGINEERING WWW.CHE.COM MAY 2008





**ROOM TO SPARE** Chromium trimers (left center) and the carboxylate linkers trimesate (left top) and terephthalate (left bottom) combine to form supertetrahedra from which the framework compounds MIL-100 and MIL-101 are constructed. Each compound contains smaller and larger nanometer-sized cages, accessible via interconnecting windows. The MIL-100 small cage is 25 Å in diameter; MIL-100 large cage, 29 Å; MIL-101 small cage, 29 Å; MIL-101 large cage, 34 Å. Cr is yellow, C is white, O is red, and H<sub>2</sub>O is green.

C&EN Chemical & Engineering News august 25, 2008 p13-16

MITCH JACOBY

Example: BASF MOFs- Rainer Zietlow -Muller-

CH4 store in MOFs for Eco Fuel World Tour ,

Volkswagen caddy- 1500 miles between fill-up

metal organic framework

European Parliament STOA 22 /3/2011  
EMRS/UPMC

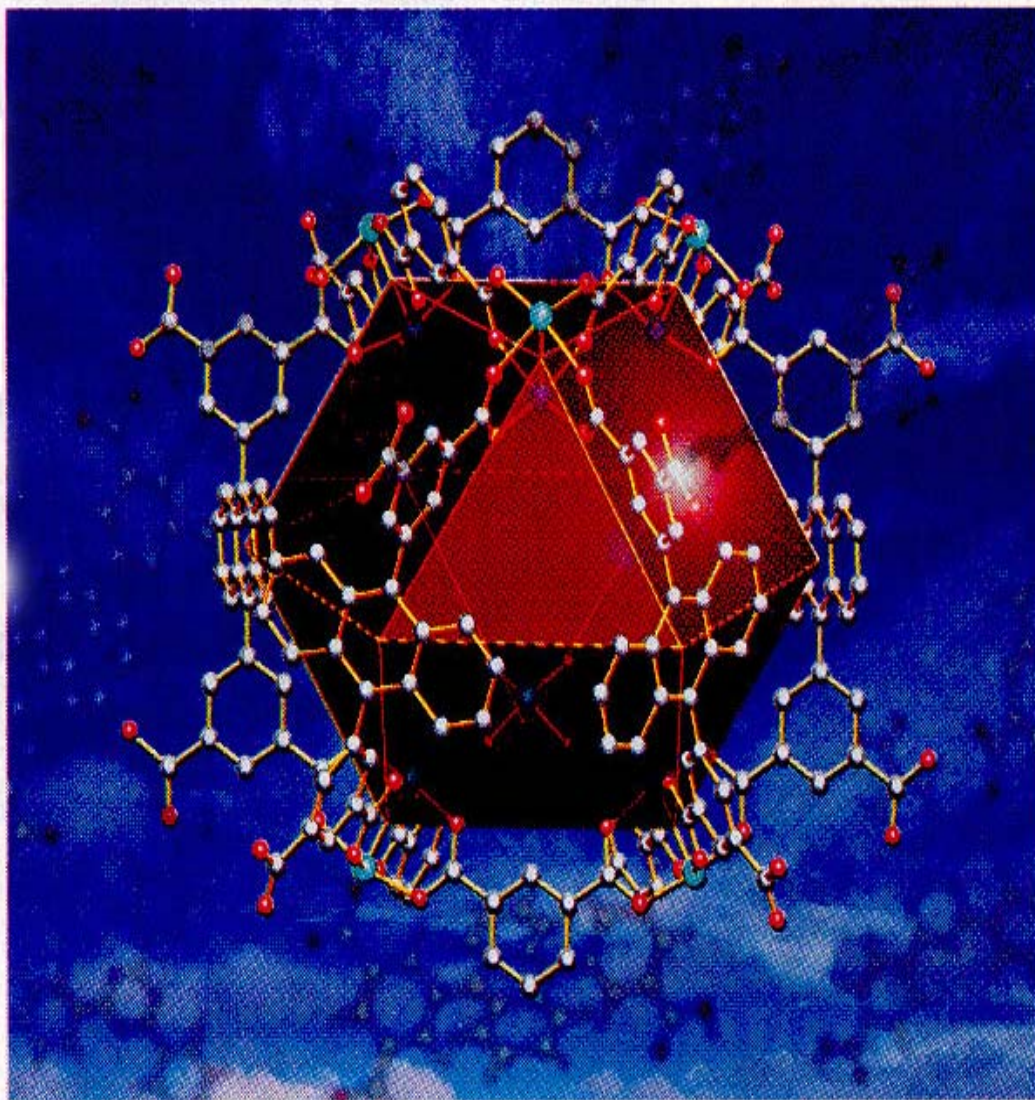
EMRS FALL MEETING  
Varsaw 13-15 sept 2010  
Symposium A

C&EN Chemical & Engineering News august 25, 2008 p13-16

MITCH JACOBY

Example: BASF MOFs- Rainer Zietlow -Muller-  
CH<sub>4</sub> store in MOFs for Eco Fuel World Tour ,  
Volkswagen caddy- 1500 miles between fill-up

**METHANE HOARDER** This framework compound, dubbed PCN-14, is composed of dicopper paddlewheel units and linkers based on an anthracene derivative. Among porous materials, PCN-14 holds the record for methane storage. Cu is turquoise, C is gray, and O is red.



DAQIANG YUAN/TEXAS A&M

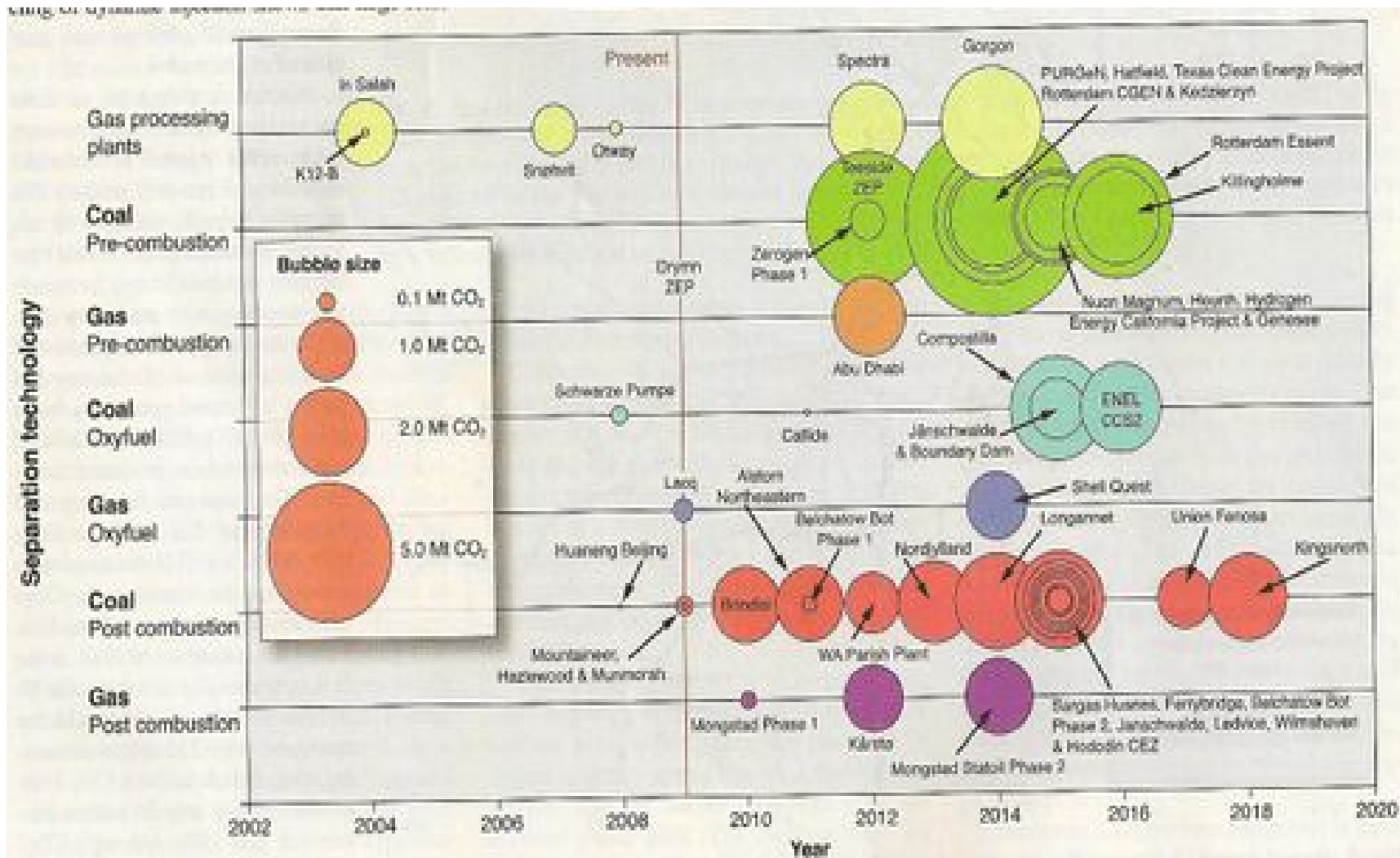
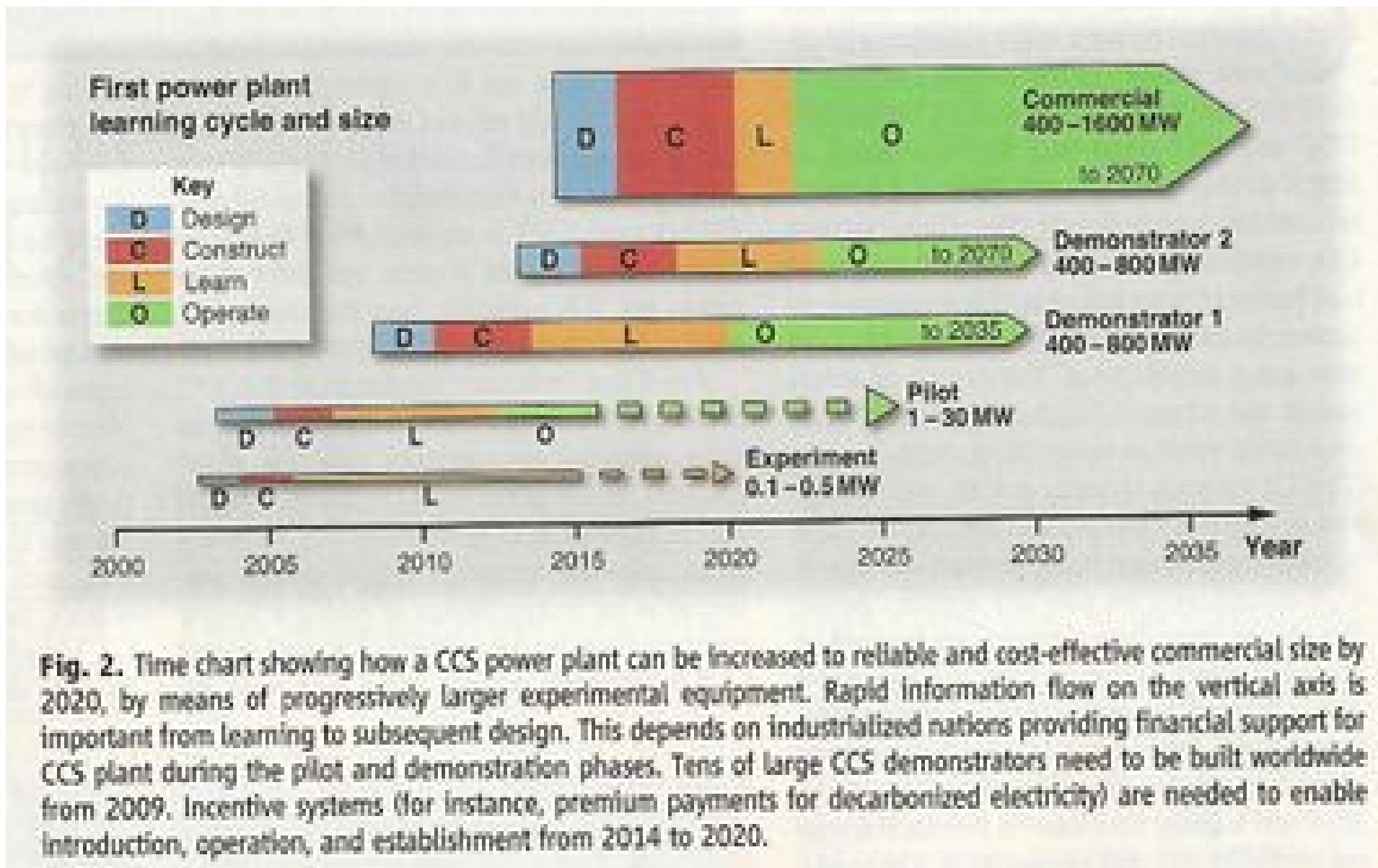


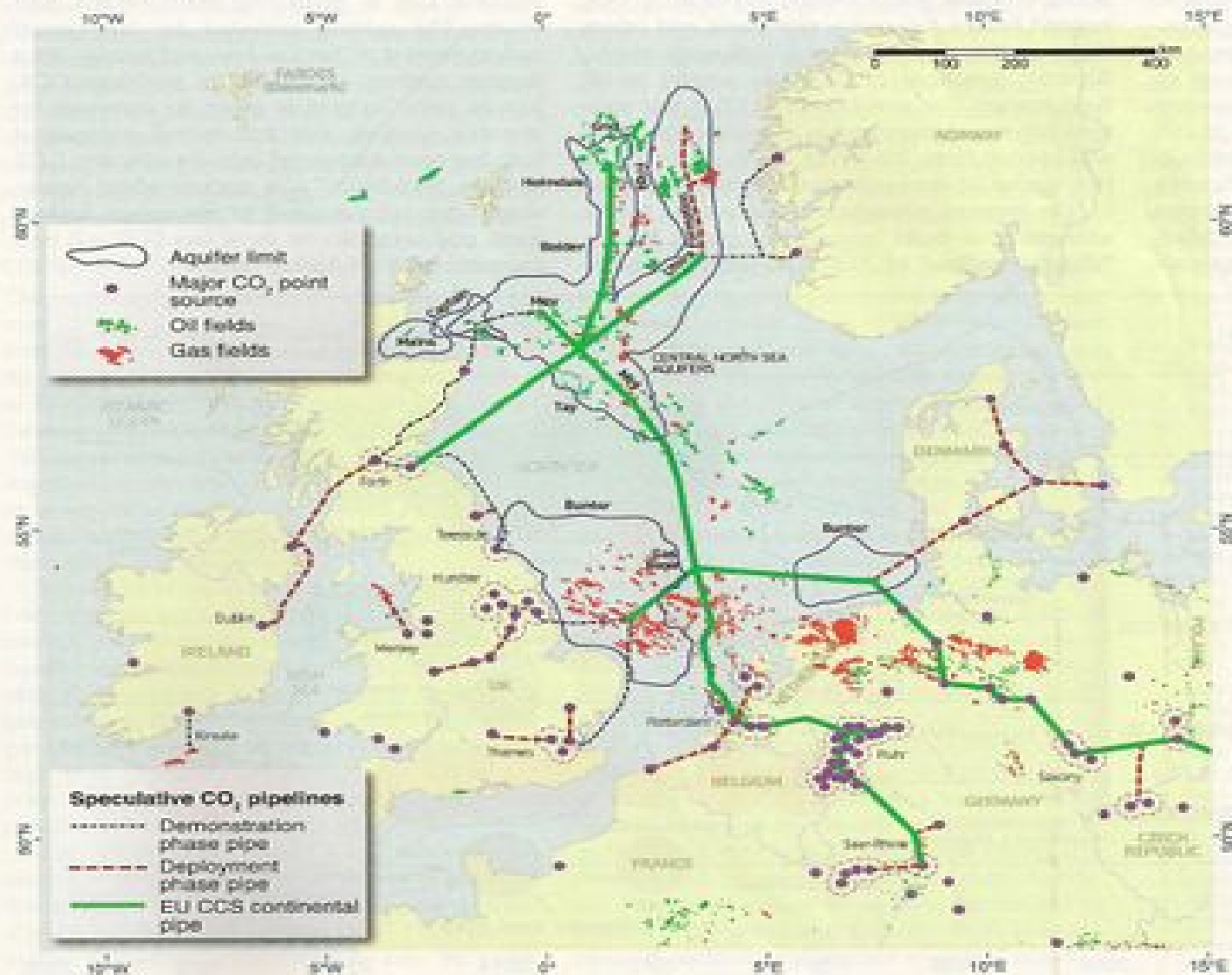
Fig. 4. Chart of large CCS demonstration projects planned worldwide, plotting calendar year against capture type and fuel. Coal and postcombustion power plants dominate. There is typically a 5-year lead time on design and construction (Fig. 2), so to operate these plants on schedule requires that projects

commence spending on design now. Few of these projects have certain funding to assist construction, and even fewer have systems to enable commercial operation. National CCS targets with worldwide coordination and exchanges of learning are needed. [Compiled by Y. Bushby (15)]



**Fig. 2.** Time chart showing how a CCS power plant can be increased to reliable and cost-effective commercial size by 2020, by means of progressively larger experimental equipment. Rapid information flow on the vertical axis is important from learning to subsequent design. This depends on industrialized nations providing financial support for CCS plant during the pilot and demonstration phases. Tens of large CCS demonstrators need to be built worldwide from 2009. Incentive systems (for instance, premium payments for decarbonized electricity) are needed to enable introduction, operation, and establishment from 2014 to 2020.

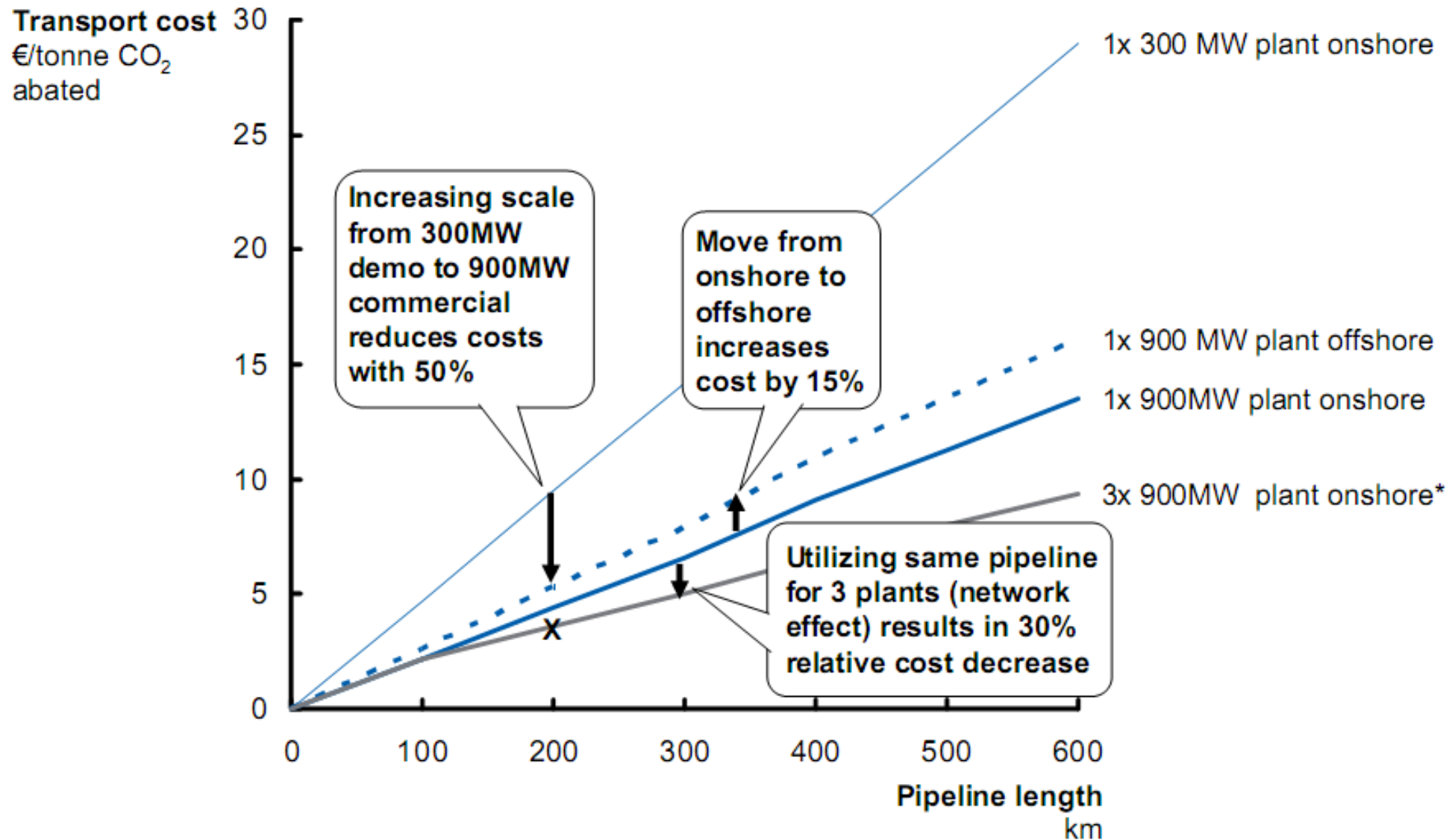
- science vol 325 25 sept 2009 p 650



**Fig. 3.** Map of northwest Europe, showing sites of emissions, saline formations, gas fields, and oil fields. CO<sub>2</sub> can be collected from clusters of large power plants and transported to storage. This transport scenario visualizes pipelines built to offshore hubs accessing large-scale storage beneath the North Sea. Such sites can be evaluated with the use of legacy hydrocarbon data and may prove to be more reliable to develop and monitor than onshore storage. [Basemap of hydrocarbon fields supplied by M. Ricketts, Wood Mackenzie]

# Scale and distance effects for transport cost

X Reference case for early commercial onshore



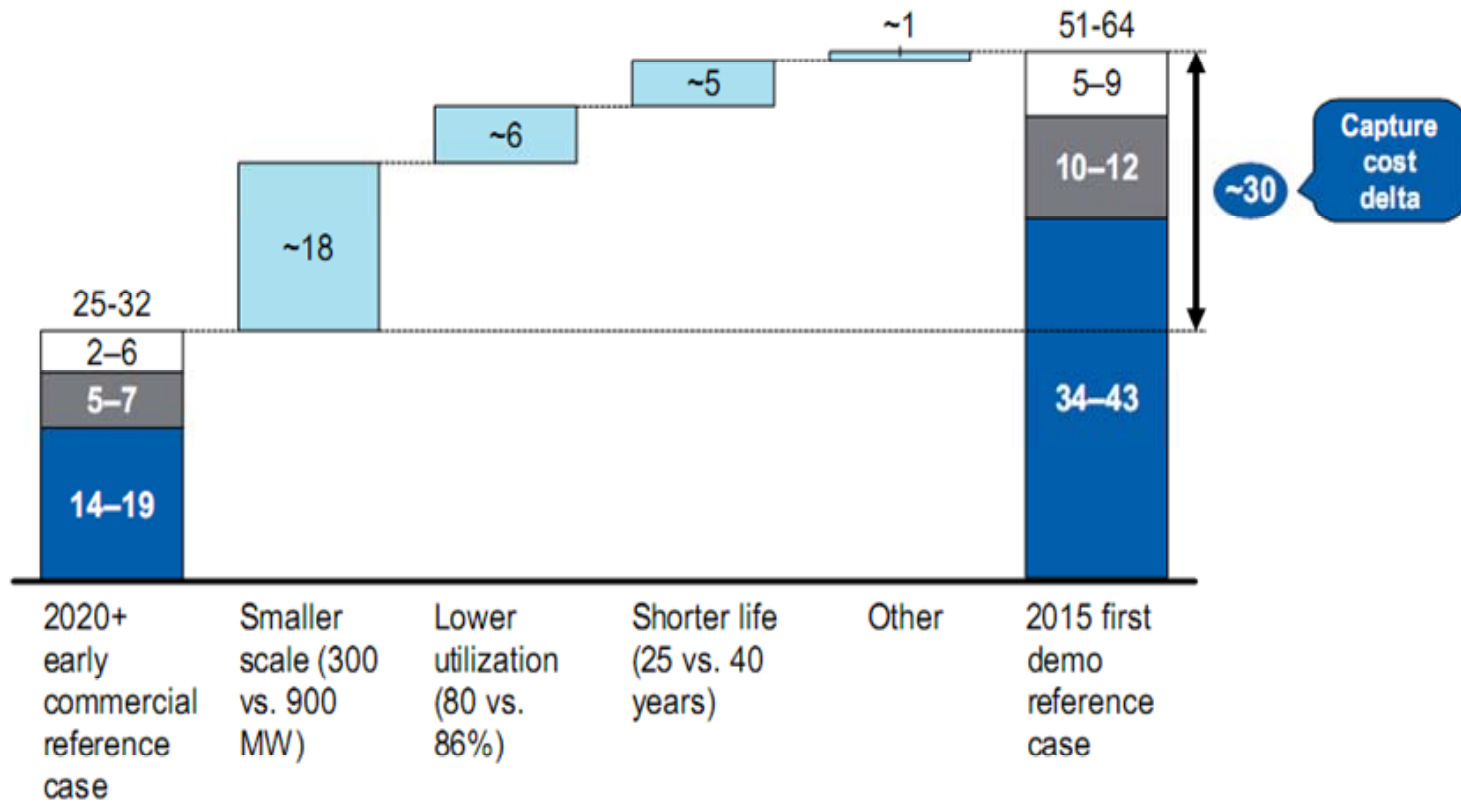
\* A network of 3 plants of 900 MW connected to shared large pipeline

Source: Team analysis

# Cost delta between demonstration and early commercial reference case – detail of capture cost delta

€/tonne CO<sub>2</sub> abated for capture

- Fuel cost
- Opex
- Capex



**2020**

**2015**

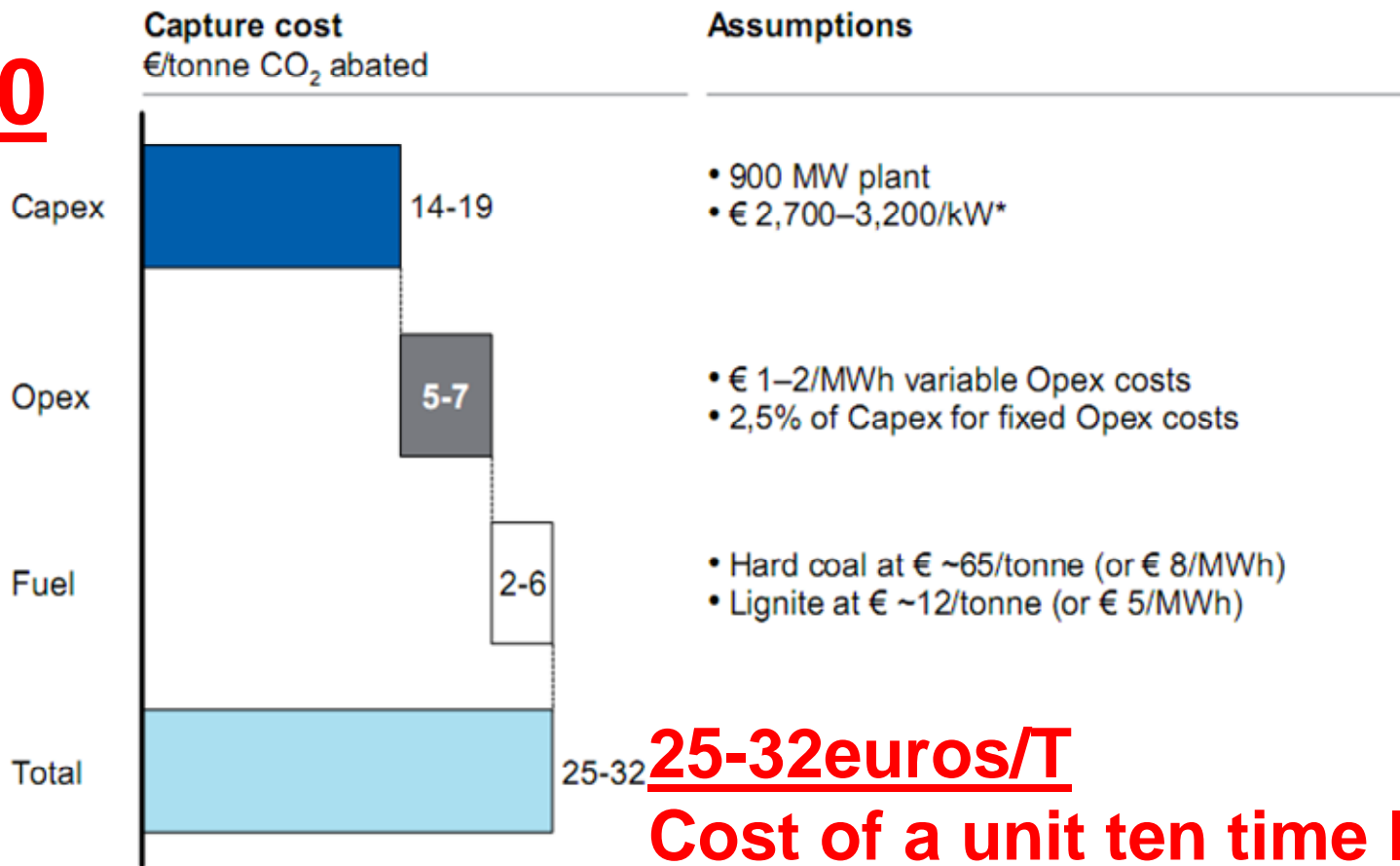
Note: Numbers in ranges may not add up due to interdependence of factors (e.g. lowest Opex may only be possible in plant with higher Capex)

Source: Team analysis

# 1 Early commercial reference case – Details of capture cost



**2020**



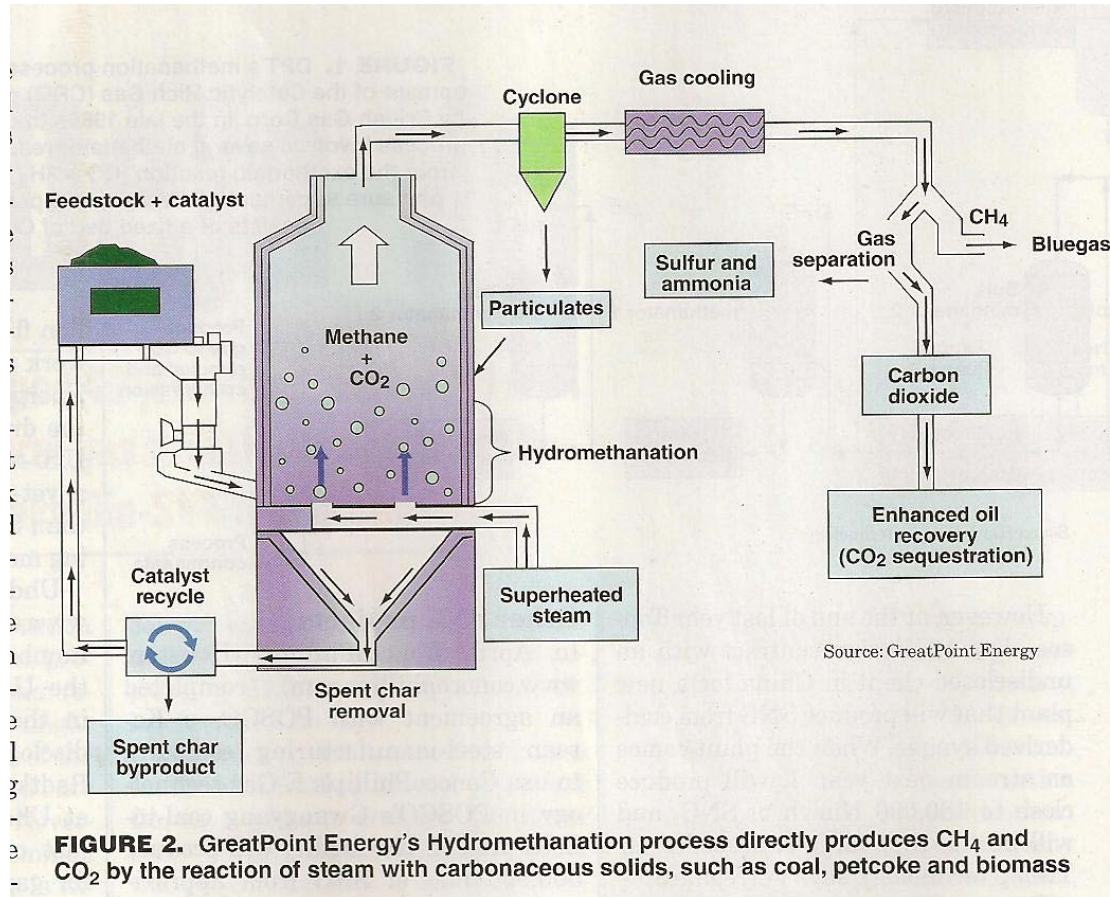
\* Assuming industrialized CCS equipment production process  
Source: Team analysis

CCS assessing economic  
Mac Kinsey 2009



# CCS in CHINA

- China's biggest coal producer : **Shenhua Group** ,propose to capture and sequestre 3.6 millions tons of CO2 per year in oil reservoirs where pressure of CO2 and its solvant properties will force hard to get oil to the surface
- Science 25 sept 2009 vol 325 p 1646



**FIGURE 2.** GreatPoint Energy's Hydromethanation process directly produces CH<sub>4</sub> and CO<sub>2</sub> by the reaction of steam with carbonaceous solids, such as coal, petcoke and biomass